

2022.10.28, Taipei, Taiwan



# Industrial Application of Continuous Chromatography by Using Supercritical Fluid as Eluent for the Separation of EPA Ethyl Ester from Fish Oil

A Conflict of Interest

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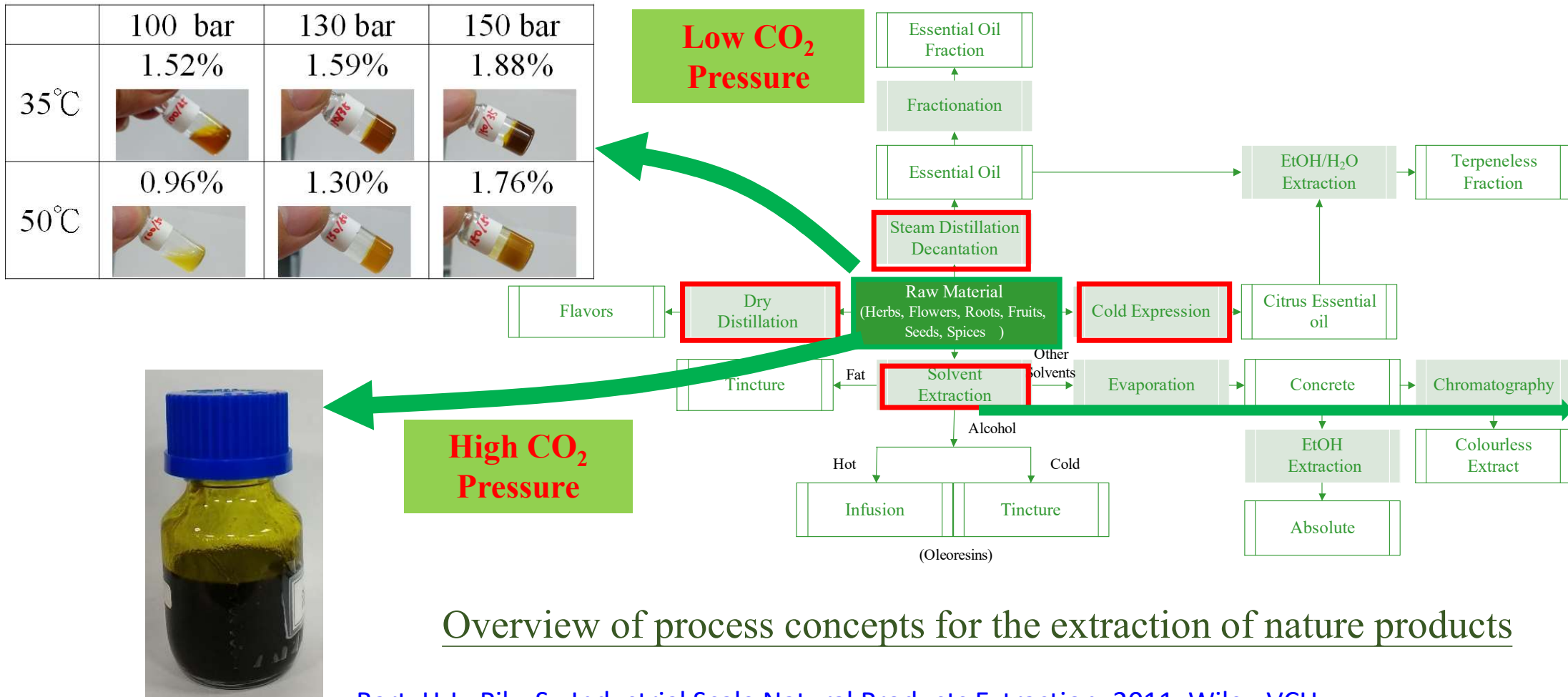


# OUTLINES

- ❑ Industrial Application of SFE
- ❑ Introduction of SMB and SFC
- ❑ Isolation of EPA from Fish Oil
- ❑ Conclusion



# □ Natural Product Processing



Bart, H.J., Pilz, S., Industrial Scale Natural Products Extraction, 2011, Wiley-VCH



# □ Process Development for Natural Products

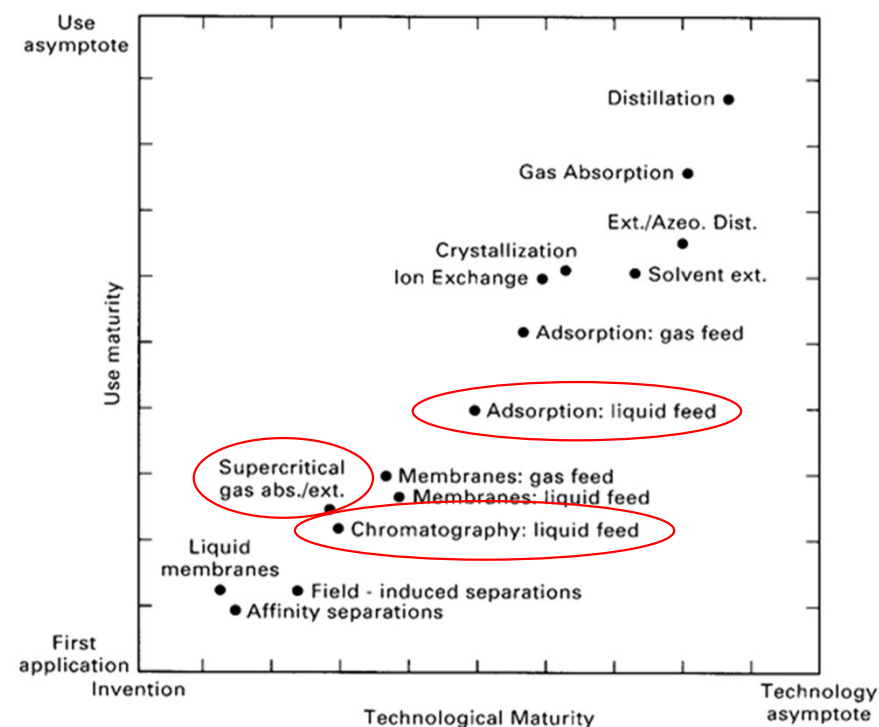
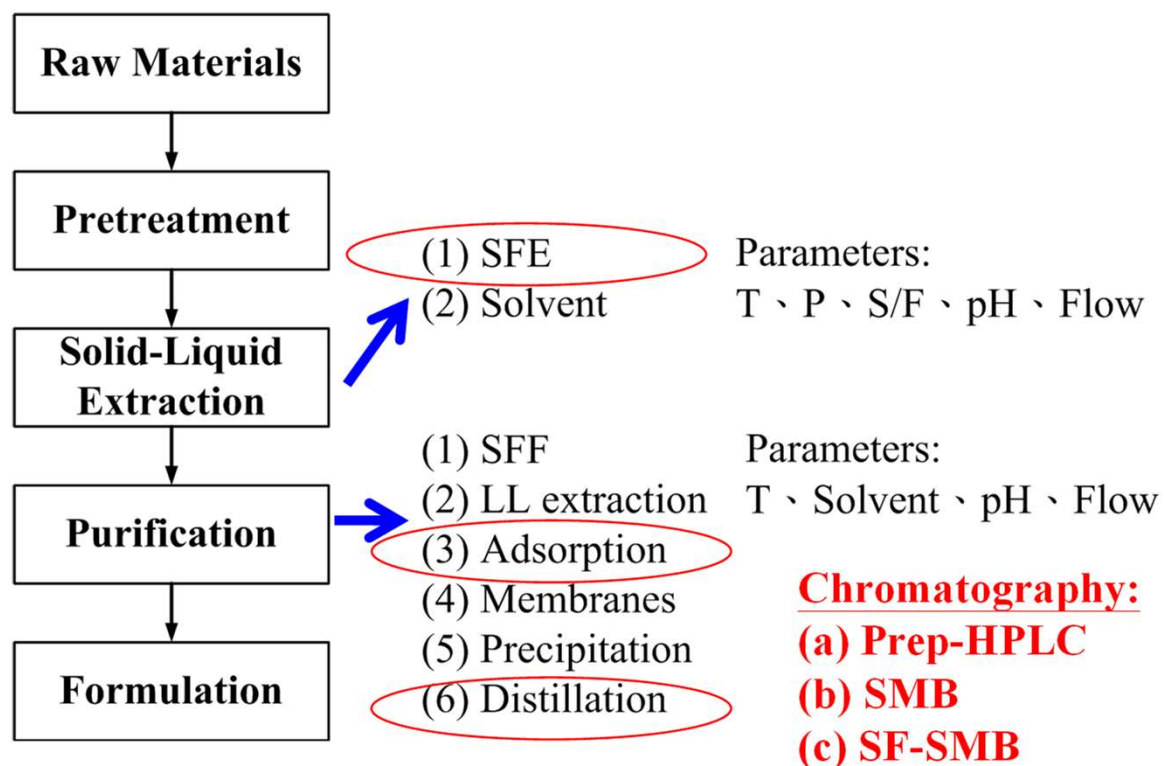


Figure 1.11 Technological and use maturities of separation processes [8].



# ❑ SFE Used in Western and Eastern World

## The Applications of SFE in West



## The Applications of SFE in East



### ITALY Decaffeination of Coffee

1992 Turn-key  
10,000 t/annual



### Korea - Special Oil Extraction



### China - Bitter Melon Seed Oil





## □ Application Diversity of SF

SF can be applied for cleaning



### Rice-Cleaning Plant Five-King Cereal Company

The first large application of SF in cleaning rather than in extraction.

If the dissolved solute is the desired products, it is called extraction.

If the impurities are removed by the SF, we call it cleaning.



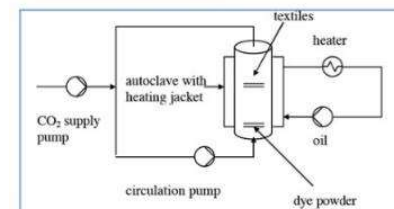
### Spain – Cork Treatment

- (1) The tannin in Cork is removed to enhance the tastetexture of redwine.
- (2) A second plant was immediately contracted to construct right after the start-up of the first plant.

Extractor volume  
 $3 \times 8,3 \text{ m}^3$



### Textiles Dying



The production of CBD oil



The production of high purity of fish oil





# □ Bioactive Compounds?

**I: SFE**



**II: MD**



SFC  
SF-SMB



**Gingerols**



中華民國/110/發明專利/I716829  
申請号或專利号: 201910390376.0

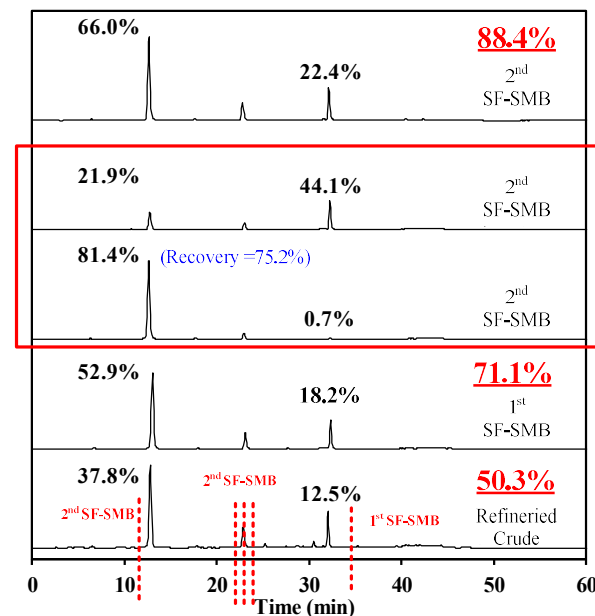
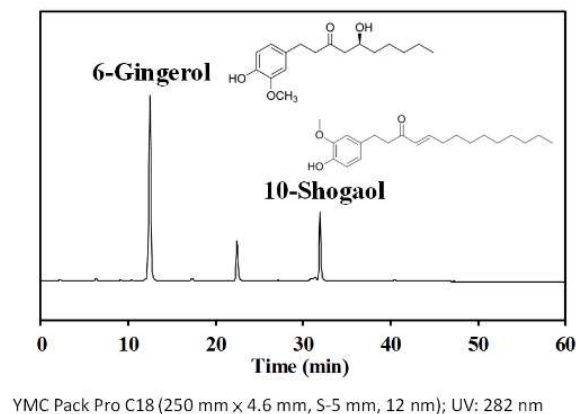
- 1<sup>st</sup> step: separate the strong retention impurities
- 2<sup>nd</sup> step: separate the weak retention impurities



Dark orange concrete

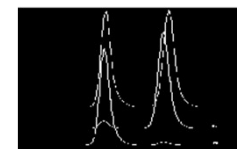


Ginger oil

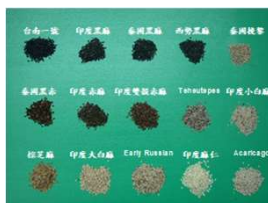




# Processes Development



Sesame



Sesame oil



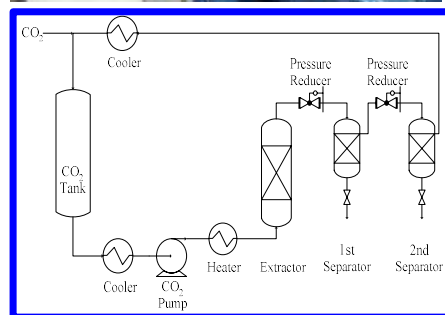
Crude Lignans



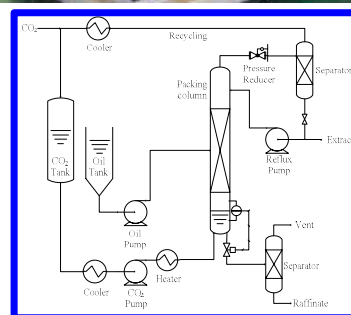
Pure Sesamolin Pure Sesamin



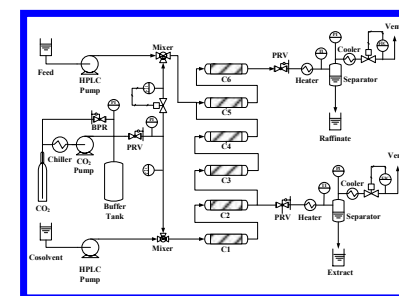
**STEP I: SFE**  
(supercritical Fluid Extraction)



**STEP II: SFF**  
(Supercritical Fluid Fractionation)



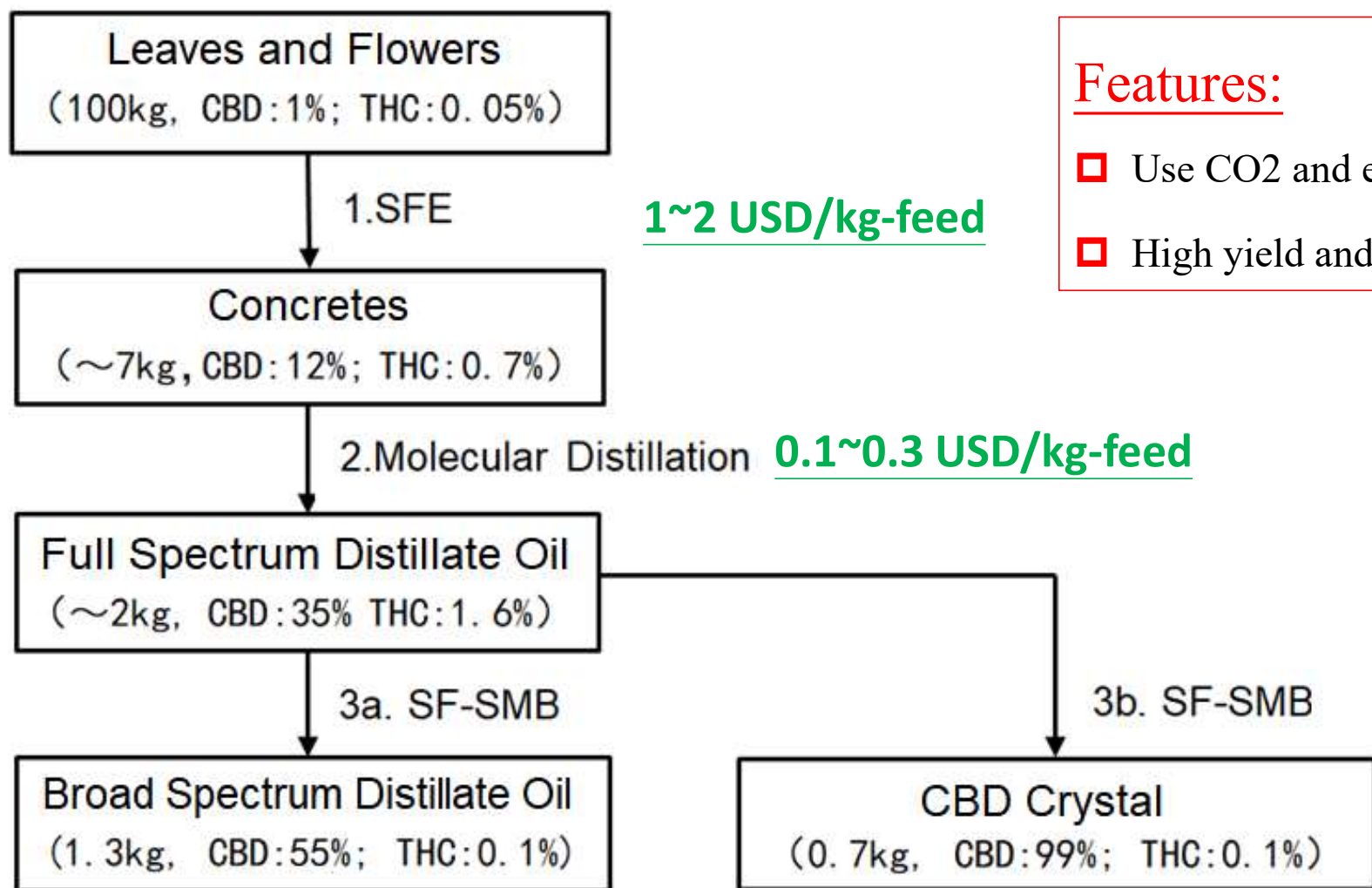
**STEP III: SF-SMB**  
(Simulated Moving Bed)



*Journal of  
Chemistry and  
Chemical  
Engineering, vol. 5,  
pp. 479-786,  
2011.06*



## □ Dry Processes for CBD oil Extraction and Purification



### Features:

- Use CO2 and ethanol.
- High yield and low energy consumption.

1~2 USD/kg-feed

0.1~0.3 USD/kg-feed

Operation Cost:  
30~60 USD/kg-feed



# OUTLINES

- Industrial Application of SFE
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# □ The Chromatography and Its Maturity in Use

## Chromatography: Chrom to Graph

Chromatography is 100 years old !

It was the russian botanist Mikhail Semenovich Tswett (1872-1919) who in 1906 first used the term chromatography: from the Greek **chroma** for color, **graphein** for writing.

Tswett (Цвѣт) is russian for color.



Pros: Selectivity  
Cons: Dilution

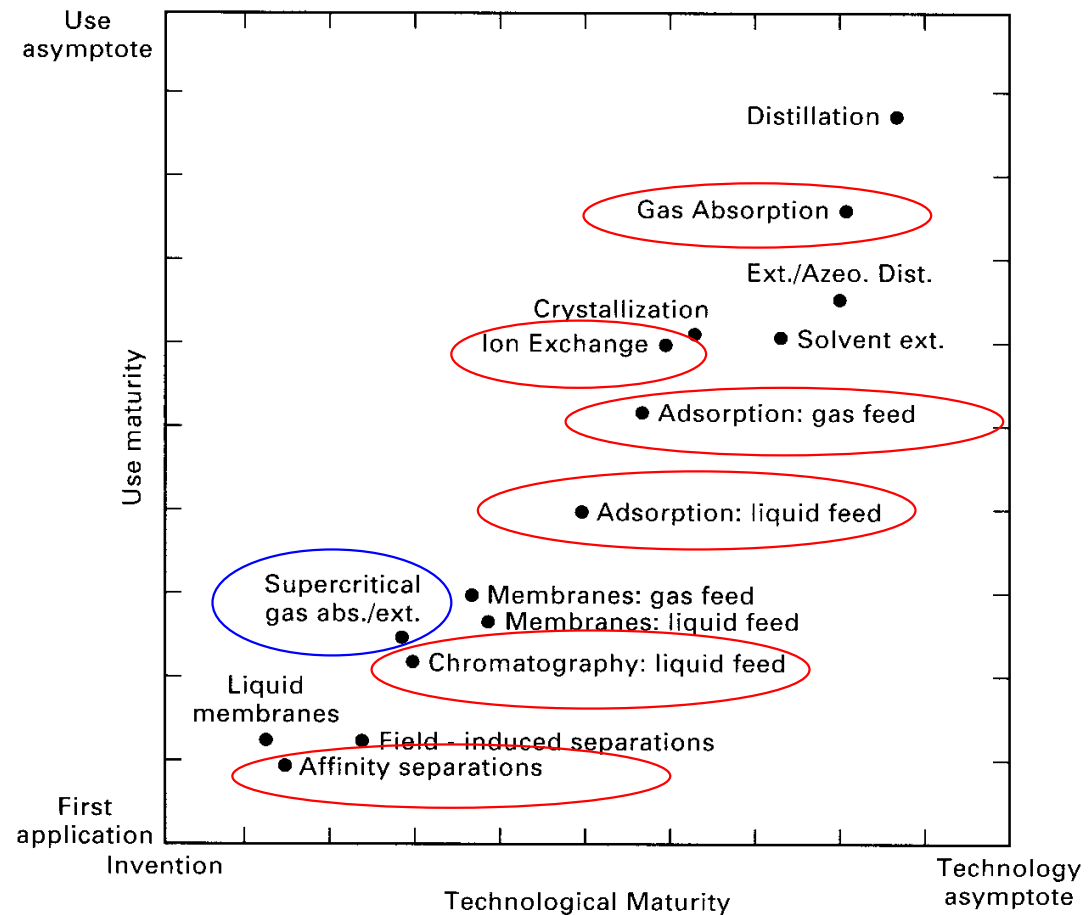
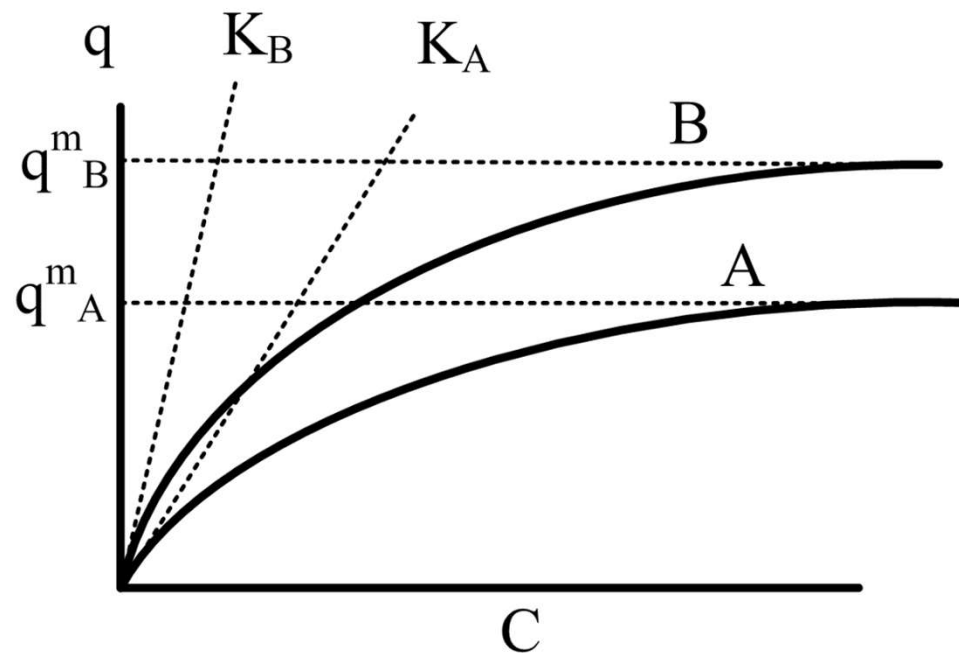


Figure 1.11 Technological and use maturities of separation processes [8].



## □ Fundamental of Chromatography

Adsorption isotherms: An equilibrium between solid and liquid phase



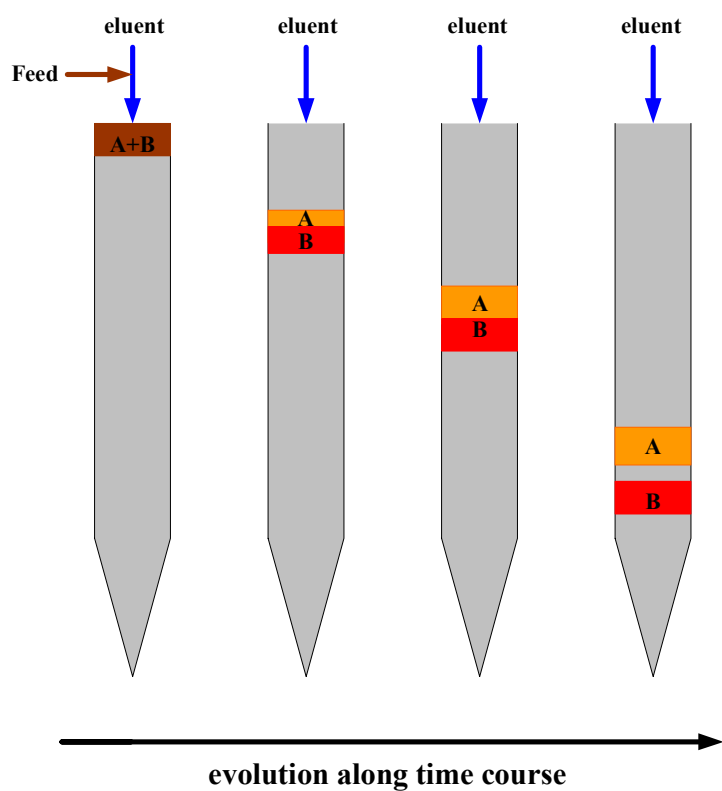
### SMB(Simulated Moving Bed) :

A technology can be used for chromatography and adsorption to increase the productivity and reduce the solvent consumption.

$$\text{Selectivity} = \frac{q_B^m}{q_A^m}, \frac{K_B}{K_A}$$



## ❑ Traditional Chromatography(Batch Operation)

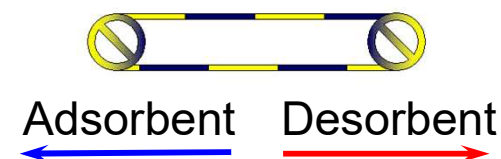
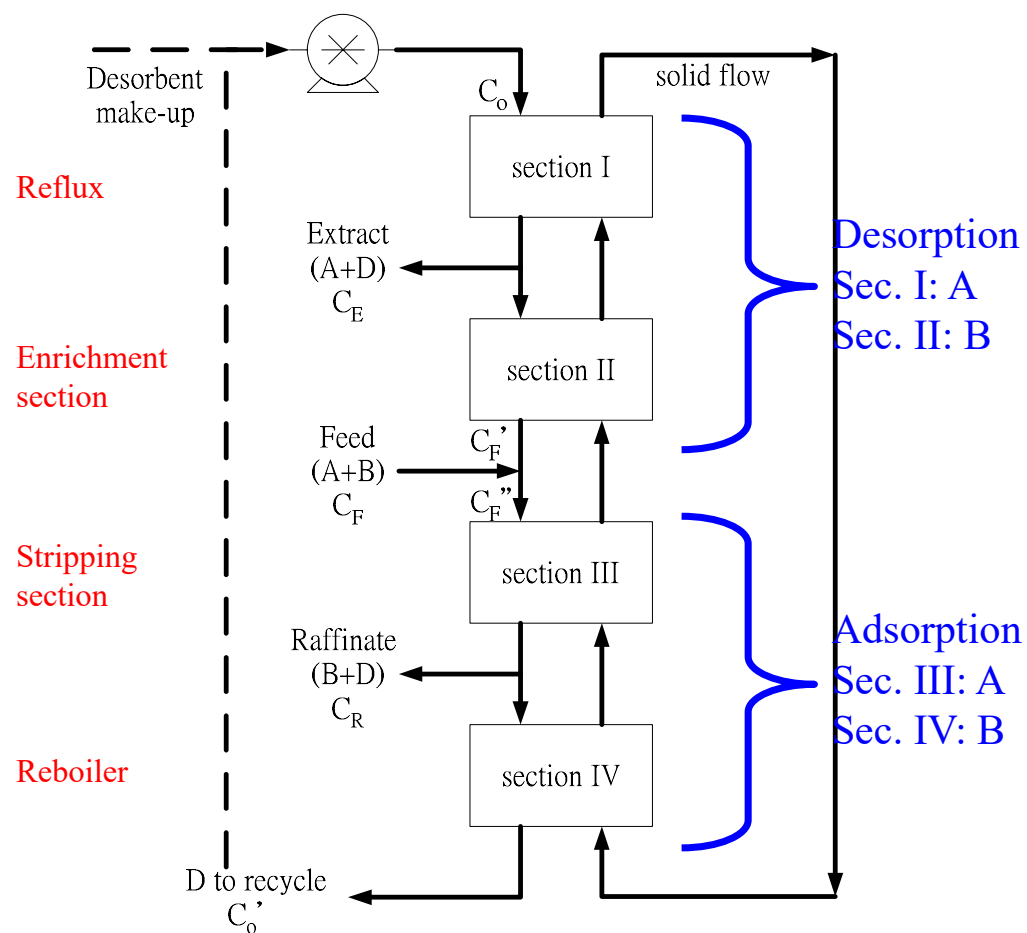


Production SFC



# Continuous Chromatography(TMB)

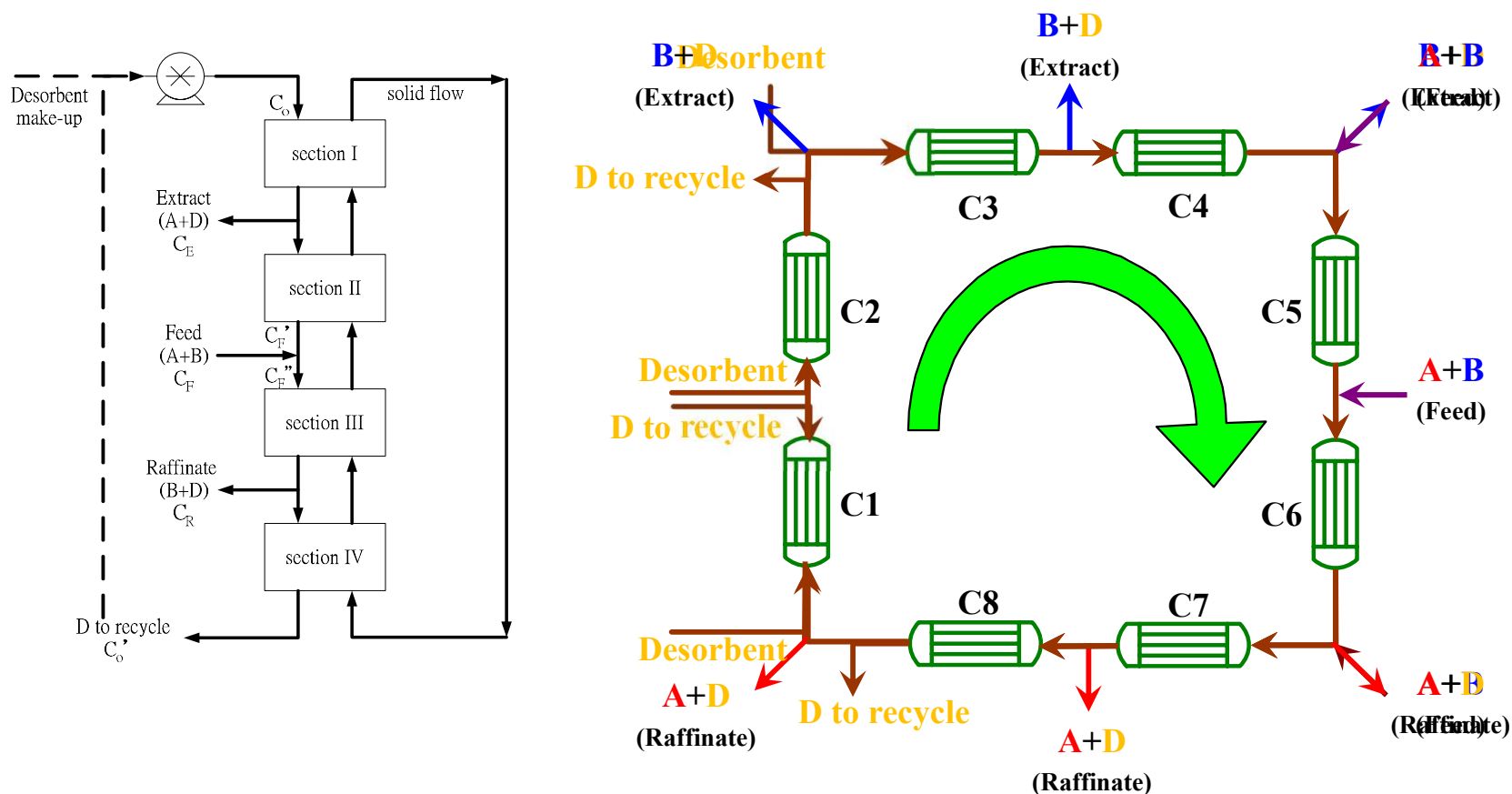
**A: Strong Retention Component**  
**B: Weak Retention Component**





## □ Continuous Chromatography(SMB)

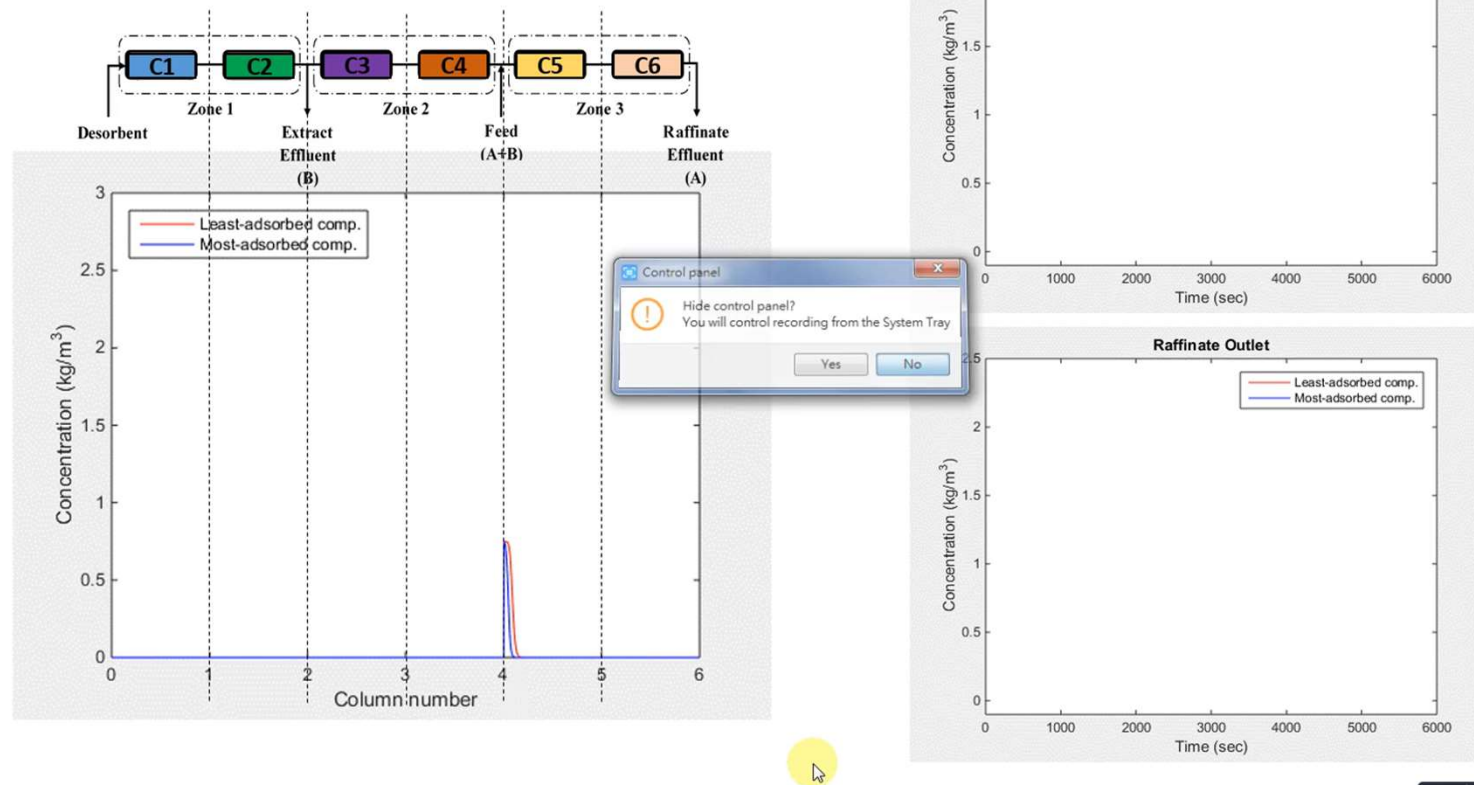
By periodically switching the ports of inlet and outlet to simulate the flow of solid in packing bed





## ❑ Periodical Change of Concentration

### Simulation Profile by CACP






## □ Comparison of HPLC and SMB

	Batch HPLC	Continuous SMB
Pros	<ul style="list-style-type: none"> <li>● High degree of freedom</li> <li>● multicomponent</li> <li>● Easy to operate</li> <li>● Easy to scale up</li> </ul>	<ul style="list-style-type: none"> <li>● Concentrated products</li> <li>● High efficient of adsorbent</li> <li>● <span style="color: red;">Low solvent consumption</span></li> <li>● <span style="color: red;">Easy to scale up</span></li> </ul>
Cons	<ul style="list-style-type: none"> <li>● Diluted products</li> <li>● High solvent consumption</li> <li>● High operating cost</li> </ul>	<ul style="list-style-type: none"> <li>● <span style="color: blue;">Complicated operation</span></li> <li>● High fixed cost</li> <li>● <span style="color: blue;">Generally for binary system</span></li> </ul>
Purities	> 85%	<span style="color: red;">&gt; 99%</span>
Recovery	> 70%	<span style="color: red;">&gt; 99%</span>
Productivity of adsorbent(kg/kg-day)	<span style="color: red;">0.01 ~ 0.1</span>	<span style="color: red;">1.0 ~ 10</span>



# □ Application of SMB in Industries

- 
- **1960s: C8 Separation in Petroleum Industry**  
Broughton and Gerhold (UOP), 1961, US patent 2985589
  - **1970s: Glucose/Fructose Separation in Sugar Refinery Industry**  
Bieser and deRosset(UOP), 1977, Detmold Germany (SAREX)
  - **1990s: Chiral Separation**  
Daicel Co. (1992) and Separex Co. (1993)
  - **1996: the first publication of SF-SMB**  
Clavier, J.Y., Nicoud, R.M., Perrut
  - **2015: the first pilot scale SF-SMB in Taiwan**  
Ming-Tsai Liang
  - **2019~2020: Full Scale of SF-SMB in Taiwan for Fish Oil**  
Ming-Tsai Liang

SMB 1960s



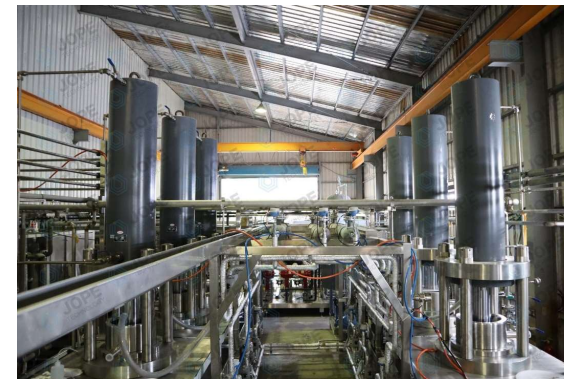
SF-SMB 2015



## Trends in 50 years:

- ✓ SP becomes smaller
- ✓ Operating pressure becomes higher
- ✓ **Process becomes greener**

SF-SMB 2019





# ❑ Application of SMB in Industries

Chromatography



SMB



SF-SMB

## Applications:

**Pharmaceutical  
Biotechnology  
Nutriceuticals**

**Bio-Medical  
Fats and Oils  
Fine Chemicals**

### Pharmaceutical:

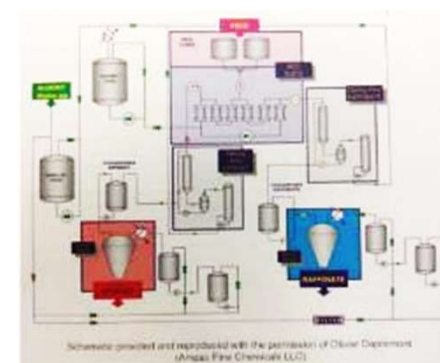
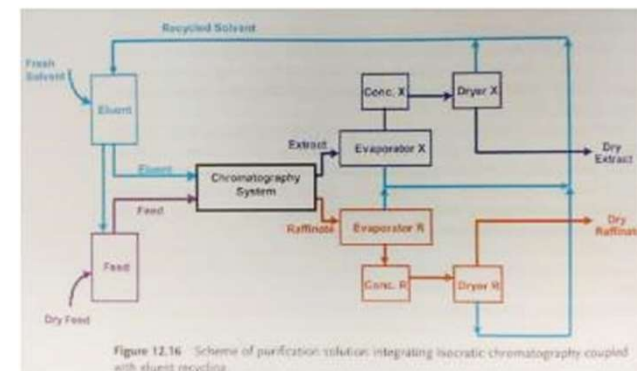
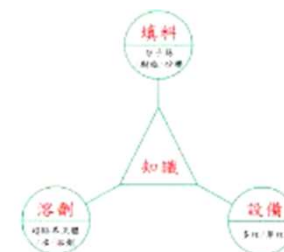
- Fractional purification of natural Tocopherols, fatty acids and phospholipids,
- Hydrophobicity parameters of drugs,
- Separation of metal ions,
- Purification and separation of vitamins A,D and E.

### Fine Chemicals:

- Separation of Chiral compound,
- Synthesis of lipid A,
- Separation of Saturated and Unsaturated fatty acids,
- Separation of Alkaloids, Fatty acid esters, Herbmedicine, Monosaccharide, Quinones, etc.

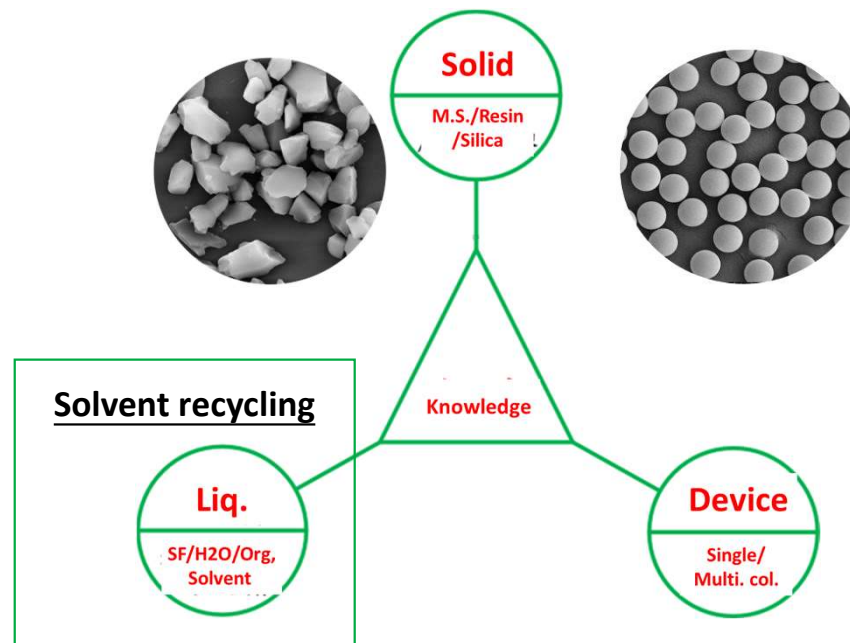
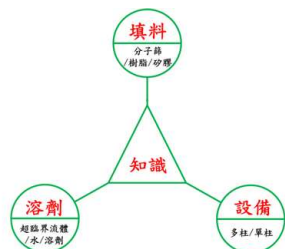
### Biotechnology:

- Purification of antibiotics from fermentation broth,
- Enzymes from Yeast extract,
- Fungous toxin Nivalenol,
- Separation of salmon sperm DNA,
- Separation of serum Proteins.





# Cost of Chromatography



**Solvent recycling**

**Liq.**

SF/H2O/Org,  
Solvent

**Solid**

M.S./Resin  
/Silica

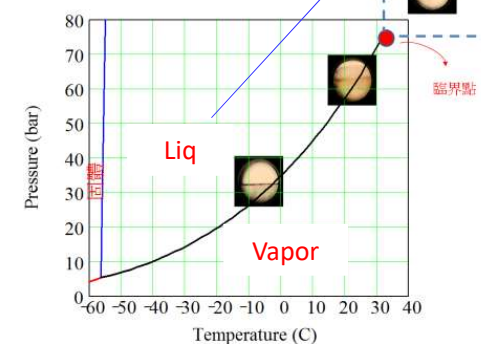
**Knowledge**

**Device**

Single/  
Multi. col.

Figure 12.16 Scheme of purification solution integrating isocratic chromatography coupled with eluent recycling.

## Fluid properties



supercritical  
fluid

臨界點

Temperature (C)

Pressure (bar)

Temperature (C)

Temperature (C)

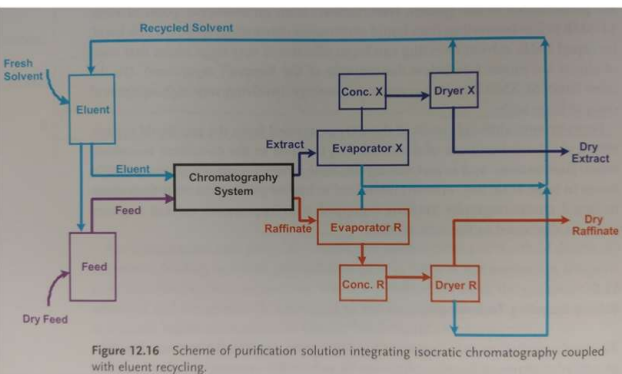
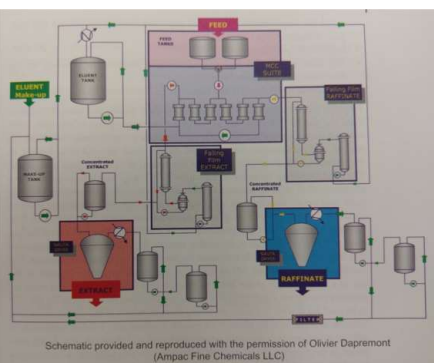


Figure 12.16 Scheme of purification solution integrating isocratic chromatography coupled with eluent recycling.



Schematic provided and reproduced with the permission of Olivier Dapremont (Ampac Fine Chemicals LLC)

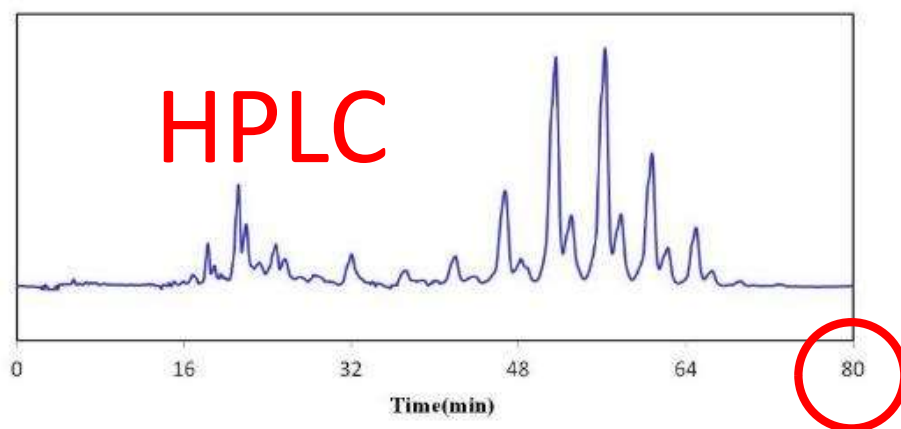
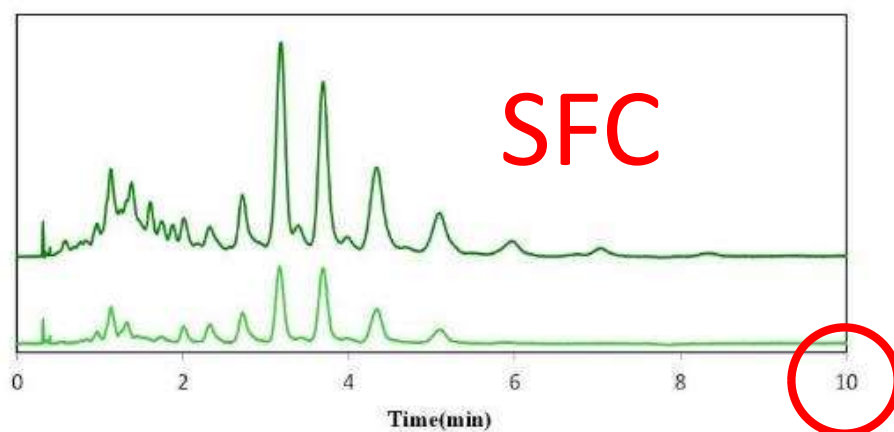




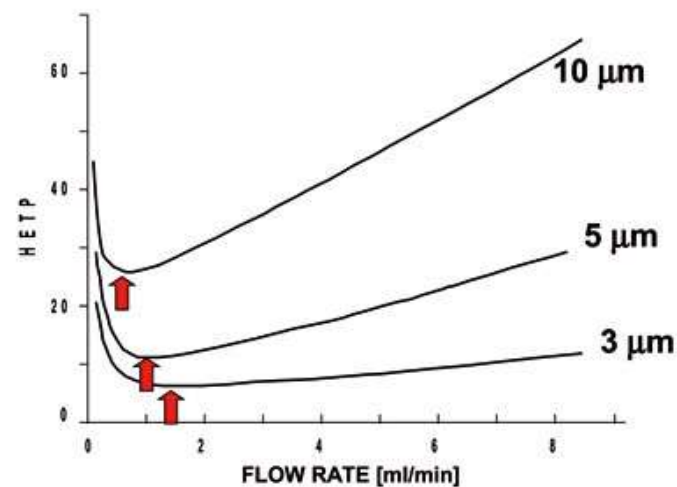
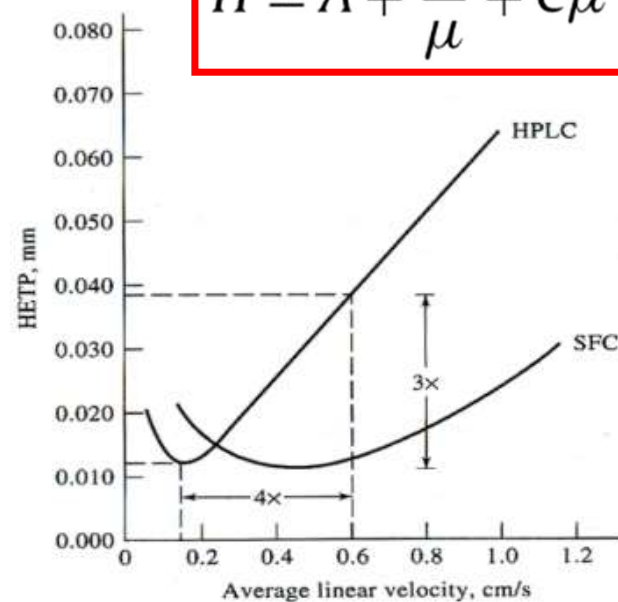
## ❑ The SFC with Packed Column

HPLC and SFC Chromatograms for Paparika red.

Shortened retention time and Higher Throughput !



$$H = A + \frac{B}{\mu} + C\mu$$





## ❑ Pros and Cons of SF-SMB

### Advantages of using SF for SMB

- ❑ can simplify the downstream concentration, because **the carbon dioxide will evaporate immediately after exposed to the ambient**
- ❑ The easy recycling of desorbent allows the **elimination of fourth section** in SMB.
- ❑ Potentially creating gradient in elution power by changing pressure and cosolvent concentration in different sections.
- ❑ It is also recognized that both reversed phase and normal phase are suitable for supercritical carbon dioxide chromatography.
- ❑ **Pressure drop** is small, the flow rate can largely increased.

### Disadvantages:

- ❑ Complicated pipe design
- ❑ High pressure operation and equipment
- ❑ Solubility is generally low for pure carbon dioxide



## ❑ Comparison of Chromatographic Methods

		Productivity*		Solvent usage	
		g racemate/kg CSP/day	g racemate/kg CSP/day	L/g racemate	L/g racemate
Batch	HPLC (recycle)	128	64	3.6	7.2
	SSR	398	199	1.73	3.46
	SFC	1600	800	0.44	0.88
Continuous	SMB	1920	960	0.16	0.32
	SF-SMB	✓	✓	✓	✓

Yields for all techniques > 95%, product purity > 98%

HPLC: Close-loop recycling chromatography

SSR: Steady state recycling chromatography

Ref: SFC 2012 short course by Miller L. and Taylor L., 2012, Oct. 3, Brussels, Belgium

- ❑ SPICA 2008: Waters merged Thar's small scale SFC ; Jasco announced re-entering SFC business; Novasep announced that 60% of chiral separation were finished by SFC.
- ❑ SPICA 2014: Novasep announces all chiral separation used SFC, and 40% of achiral separation used SFC.
- ❑ SPICA 2012: Lilly published that 98% of achiral chromatography can be finished by Hilic or 2-EP.



## ❑ Cost Comparison among Chromatographic Methods

### Cost for production of fish oil by using different chromatography

Cost	SF-SMB	SMB	HPLC
Feed stock	10%	10%	10%
Personnel Cost	32%	38%	48%
depreciation	30%(28/2)	18%(16+2)	9%(8+1)
Solvent/Energy/Solid	17%(7/5/5)	100%(70/25/5)	400%(280/100/20)
Housing and Overhead	11%(4/7)	11%	11%
	100%	177%	478%

→ The saving mainly comes from the solvent recycling



## ❑ The State of the Art of SMB

### SMB:

1950's- SMB begins with UOP

1970's- SMB for sugar industries

1993- First report for pharmaceutical industry

1997- First chiral application run at UCB on a production scale

2001- the first FDA inspection of an SMB unit for an API

1990's – Aerojet, Lundbeck, Carbogen and Bayer

2003- Aldrich invests in plant in Buchs

2006- Aerojet built up a 100 cm unit

2016-Novasep built up a 120 cm fish oil

### SFC and SF-SMB:

1962- first report of SFC by Klesper et al.

1970's – CO<sub>2</sub> become preferred fluid for packed column

1980's - open tubular capillary columns became popular

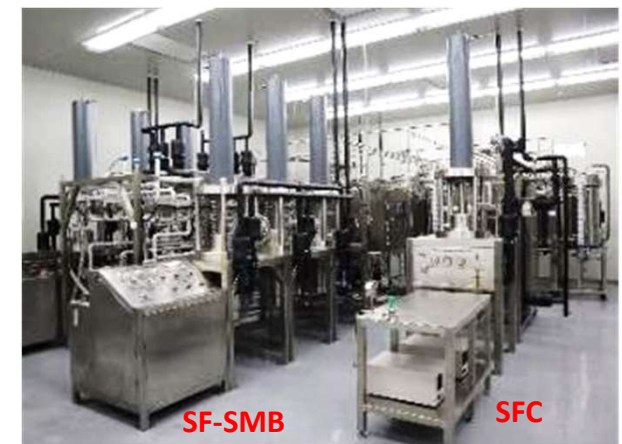
1990's – packed column regained popularity and began widely in chiral separation

**1996- first report of SF-SMB by Dr. Perrut**

**2015- First pilot SF-SMB 80mmx8 by JOPE**

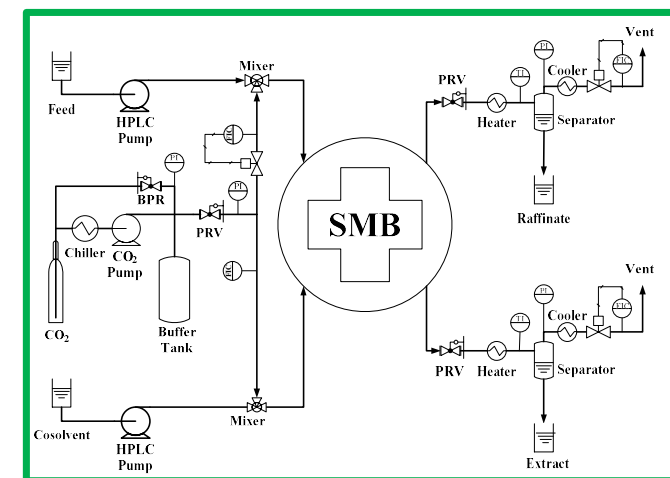
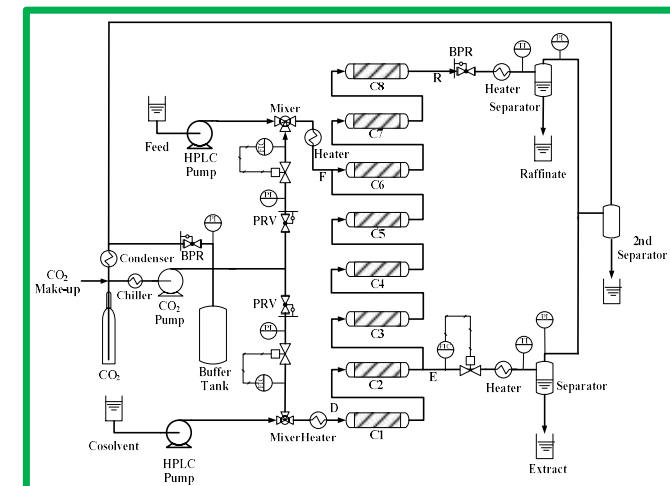
**2019- The largest SF-SMB 300mmx6 and SFC 600mm for CBD**

**2020- First Industrial Application in Taiwan for Fish Oil**





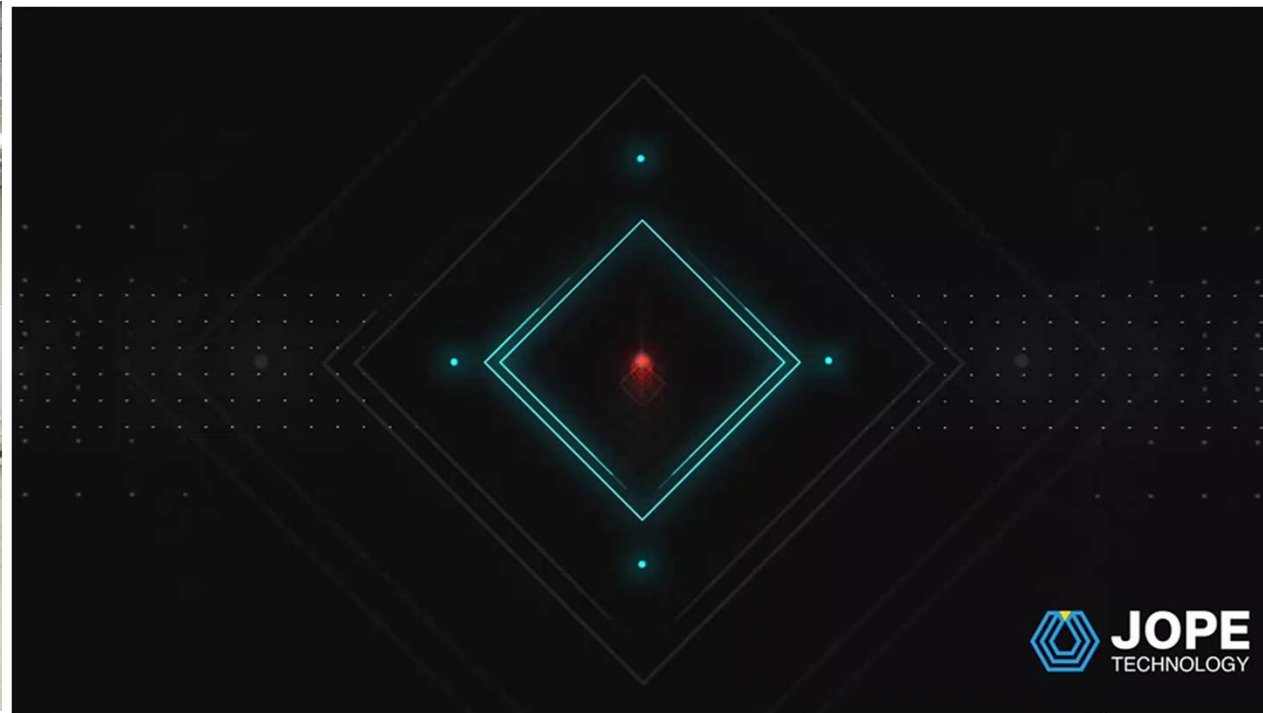
# □ An Overview of Production Scale SF-SMB





## ❑ Construction of SF-SMB

### ◆ SF-SMB 300mmx6 and SFC 600mm





# OUTLINES

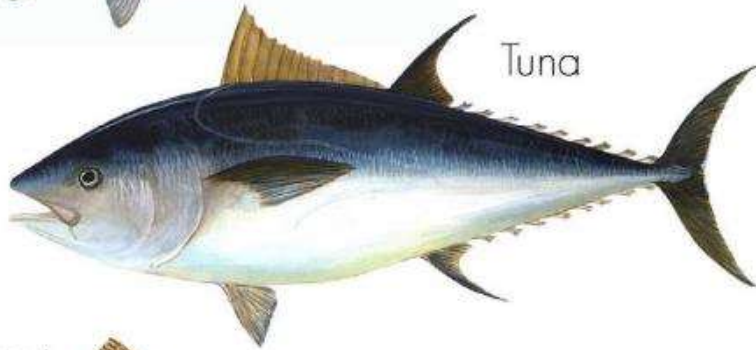
- Industrial Application of SFE
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## ☐ Oily Fish from Chile and Peru



Salmon



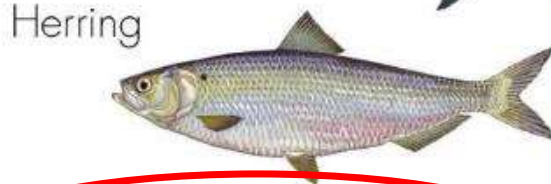
Tuna



Trout



Mackerel



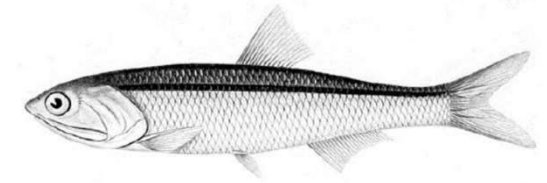
Herring



Sardine



Anchovy



Anchovy in Taiwan





## Free Fatty Acids Composition in Fish Oil

Fatty acid	Farmed Atlantic Salmon	Tuna	Jack mackerel	Herring	Atlantic cod liver	Atlantic menhaden	South American anchovy	Capelin	Sardine	Seal	Krill
14:0 (myristic acid)	4.2	3.9	7.3	7	3.3	7.3	7.5	7	8	5.0	9.5
16:0 (palmitic acid)	15.7	17.6	15.7	16	13.4	19	17.5	10	18	11.3	20.8
16:1 n-7	5.1	5.4	5.1	6	9.6	9.1	9	10	10	14.3	9.9
18:0 (stearic acid)	4.2	4.1	3.1	-	2.7	4.2	4	-	-	1.1	0.9
18:1 n-9	16.5	12.4	9.9	13	23.4	13.2	11.6	14	11	22.3	10.5
18:1 n-7	3.5	2.4	2.9	-	-	-	-	-	-	4.9	10.3
20:1 n-9	3.3	1.3	8.3	12	7.8	2	1.6	17	4	7	<1
22:1	2.5	0.5	5.8	20	5.3	0.6	1.2	14	3	2.3	<0.5
18:2 n-6 <sup>1)</sup> (LA)	6.6	1.9	1.7	-	-	1.3	1.2	-	-	1.1	2.3
20:5 n-3 <sup>2)</sup> (EPA)	7.1	12.4	10.9	5	11.5	11	17	8	18	6.6	18.2
22:6 n-3 <sup>3)</sup> (DHA)	15.7	27.8	11.5	6	12.6	12.6	8.8	6	9	8.7	9.5
22:5 n-3 <sup>4)</sup> (DPA)	3.9	1.7	2	-	1.6	1.6	1.6	-	-	4.4	-
<b>Total n-3<sup>5)</sup> LC-PUFA</b>	<b>26.7</b>	<b>41.9</b>	<b>24.4</b>	<b>11</b>	<b>25.7</b>	<b>22</b>	<b>27.4</b>	<b>14</b>	<b>27</b>	<b>19.7</b>	<b>27.7</b>

<sup>1)</sup> LA – linoleic. <sup>2)</sup> EPA – eicosapentaenoic. <sup>3)</sup> DHA – docosahexaenoic acid. <sup>4)</sup> DPA – docosapentaenoic acid.

<sup>5)</sup> LC-PUFA: long chained polyunsaturated fatty acids.







## API from Fish Oil: the separation of EPA and DHA

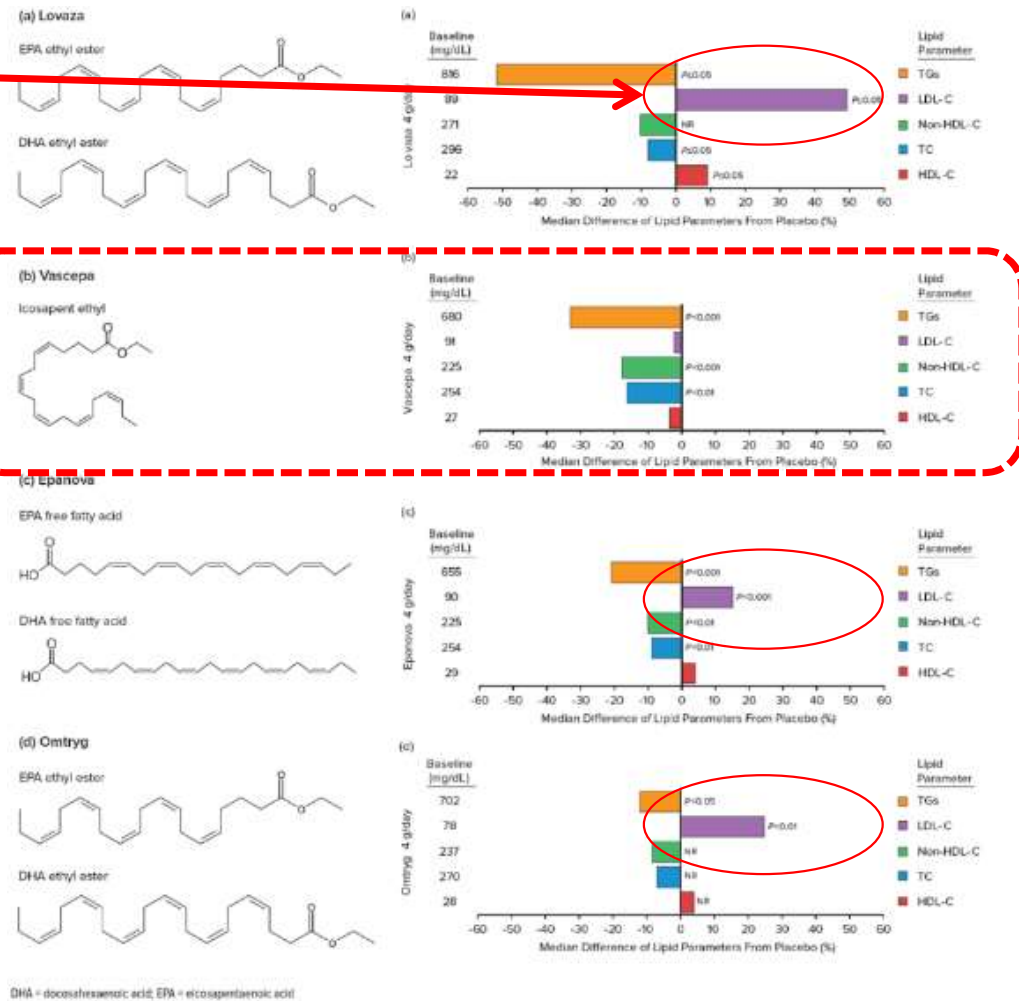
DHA leads the increase of LDL

- 1) Crandell JR, Tartaglia C, Tartaglia J., Lipid effects of switching from prescription EPA+DHA (omega-3-acid ethyl esters) to prescription EPA only (icosapent ethyl) in dyslipidemic patients, *Postgraduate Medicine*, 128 (2016) 859-864
- 2) Matthew K. Ito, A Comparative Overview of Prescription Omega-3 Fatty Acid Products, *Pharmact and Therapeutics*, 40 (2015) 826-836
- 3) Tajuddin N, Shaikh A, Hassan A. Prescription omega-3 fatty acid products: considerations for patients with diabetes mellitus, *Diabetes Metab Syndr Obes.*, 19 (2016) 109-118
- 4) Sperling LS, Nelson JR., History and future of omega-3 fatty acids in cardiovascular disease, *Curr Med Res Opin.*, 32 (2016) 301-11
- 5) Eliot A. Brinton, R. Preston Mason, Prescription omega-3 fatty acid products containing highly purified eicosapentaenoic acid (EPA), *Lipids in Health and Disease*, 16 (2017) 1-13

Vol. 40 No. 12 • December 2015 • P&T® 827

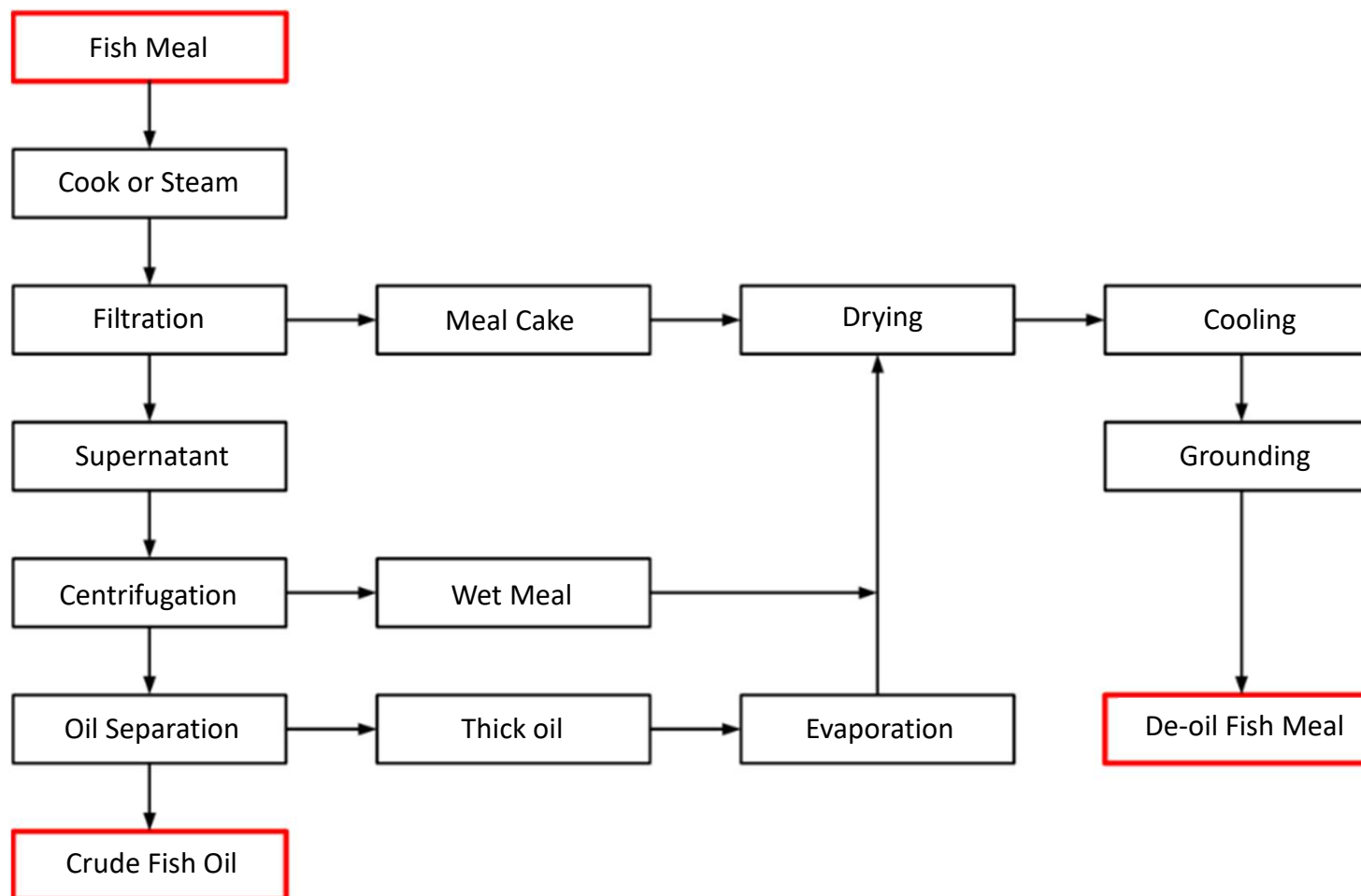
A Comparative Overview of Prescription Omega-3 Fatty Acid Products

Matthew K. Ito, PharmD, FCCP, FNLA, CLS



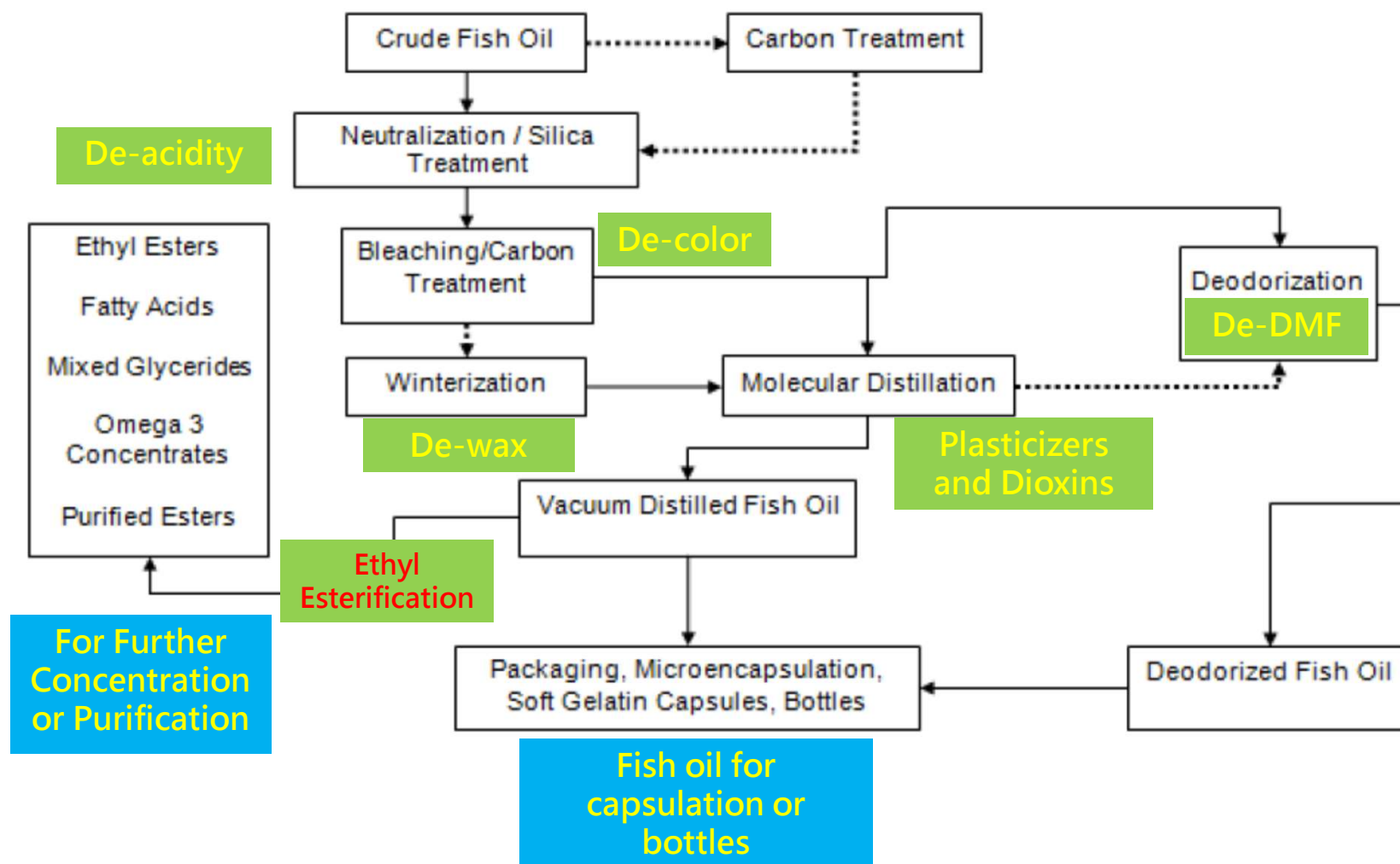


## ❑ Fish Oil Extraction





## ❑ Fish Oil Refinery





# Concentration and Isolation of Fish Oil

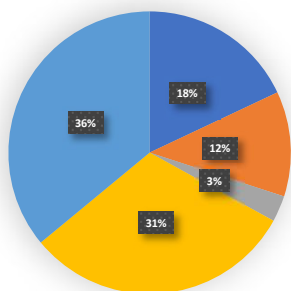
Chromatography to isolate EPA

SFF or Vacuum Distillation to separate DHA and EPA

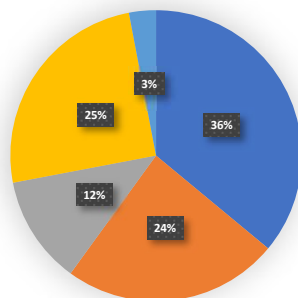
Molecular Distillation to remove C16 and C18 FA

Crystallization to remove saturated and mono-unsaturated FA

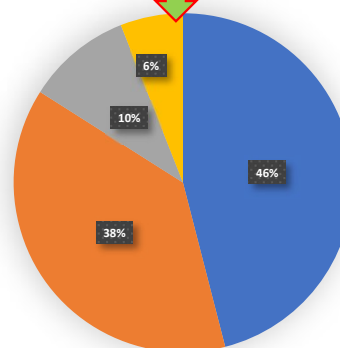
■ EPA  
■ DHA  
■ Else Omg-3  
■ Non Omg-3  
■ Others



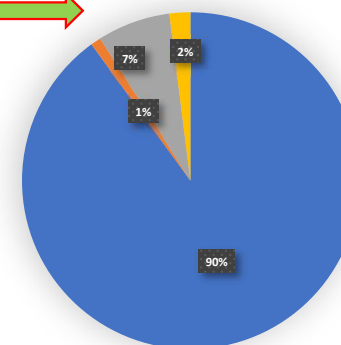
Original: EPA/DHA = 18/12



36/24



46/38



EPA~90



EPA95				
Peak#	Ret. Time	Area		
1	1.625	86123099		
2	2.053	260633		
3	2.514	1495	0.12%	
4	14.616	15970	1.30%	C18:4, ω-3(SDA)
5	14.912	1258	0.10%	
6	17.379	2915	0.24%	
7	18.049	7546	0.62%	C20:4, ω-6
8	19.119	3952	0.32%	C20:4, ω-3
9	19.671	1172355	95.61%	C20:5, ω-3(EPA)
10	21.706	3325	0.27%	C21:5, ω-3
11	22.047	6225	0.51%	
12	24.836	9716	0.79%	C22:6, ω-3(DHA)
13	26.26	1421	0.12%	



## □ Production Technologies for EPA 97



DYNES  
Biotech.:



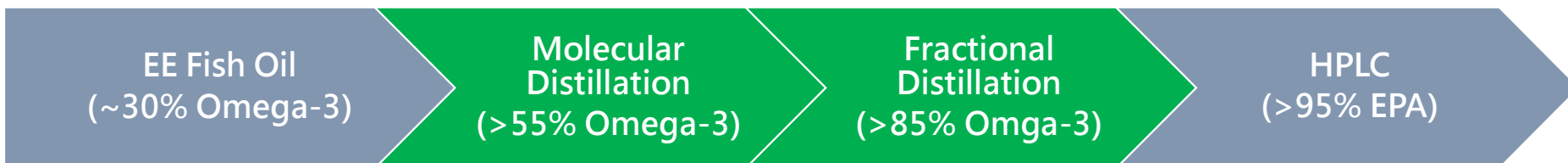
KD-  
Pharma:



Novasep:



Nissui:





## □ EPA 97 by liq-SMB

### Novasep:



Varicol® 5-1200mm I.D./2 single-column chromatography systems of 1200 mm





## □ An overview of DYNES Biotech.

DYNES  
Biotech.:





## ❑ Vascepa and its generic drugs and Nutraceuticals

### Amarin (prescription)



### Epadel (prescription, OTC)



### Hikma (prescription)



### Dynes (Food Grade)



### EPA API Manufactures:

#### Generic Drugs:

- Manufacturer: **APOTEX**  
Approval date: June 30, 2021
- Manufacturer: **DR REDDYS**  
Approval date: August 7, 2020
- Manufacturer: **HIKMA**  
Approval date: May 21, 2020

	Manufacturer	Launched	Technologies
Amarin (Brand Drug)	Nisshin(Japan)	2012	Vacuum Distillation + HPLC
	Chemport(Korea)	2012	Vacuum Distillation + HPLC
	Novasep(French)	2015	SMB + HPLC
	KD Pharma(German)	2019	SMB + HPLC
	BASF(German)	2013	SMB + HPLC
Generic	CCSB(Taiwan)	2020	Metal Complexed Extraction
Food Grade	DYNES(Taiwan)	2021	SF-SMB

Source: USFDA, Company filings, Jefferies



□ EPA 97 API by CO<sub>2</sub>+MeOH; EPA 95 Nutraceuticals by CO<sub>2</sub>+EtOH



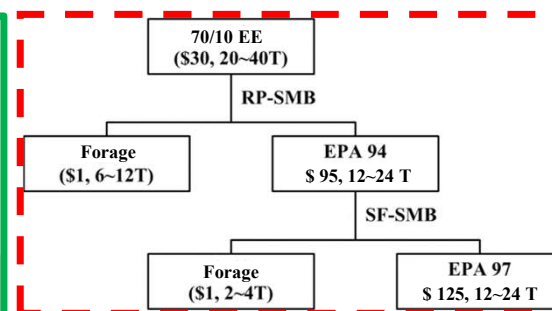
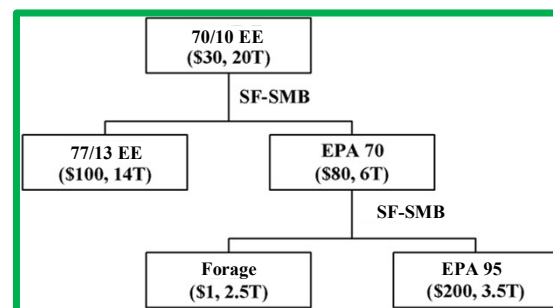
Nutraceuticals



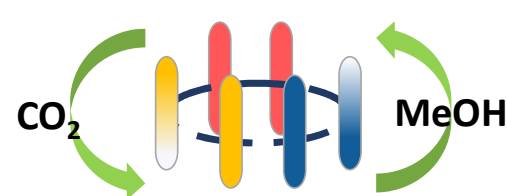
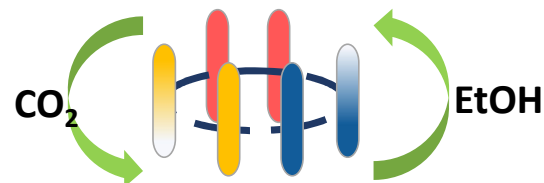
Pharmaceuticals



EPA95				
Peak#	Ret. Time	Area		
1	1.625	86123099		
2	2.053	260633		
3	2.514	1495	0.12%	
4	14.616	15970	1.30%	C18:4, ω-3(SDA)
5	14.912	1258	0.10%	
6	17.379	2915	0.24%	
7	18.049	7546	0.62%	C20:4, ω-6
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10	21.706	3325	0.27%	C21:5, ω-3
11	22.047	6225	0.51%	
12	24.836	9716	0.79%	C22:6, ω-3(DHA)
13	26.26	1421	0.12%	



EPA97				
Peak#	R.Time	Area		
1	1.627	56539411		
2	2.079	385469		
3	9.183	1152	0.10%	
4	13.321	2127	0.18%	
5	13.79	1363	0.12%	
6	14.112	2900	0.25%	
7	14.756	4534	0.38%	C18:4, ω-3(SDA)
8	18.196	5126	0.43%	C20:4, ω-6
9	19.265	1795	0.15%	C20:4, ω-3
10	19.814	1156678	98.01%	C20:5, ω-3(EPA)
11	22.196	1747	0.15%	
12	24.984	2701	0.23%	C22:6, ω-3(DHA)





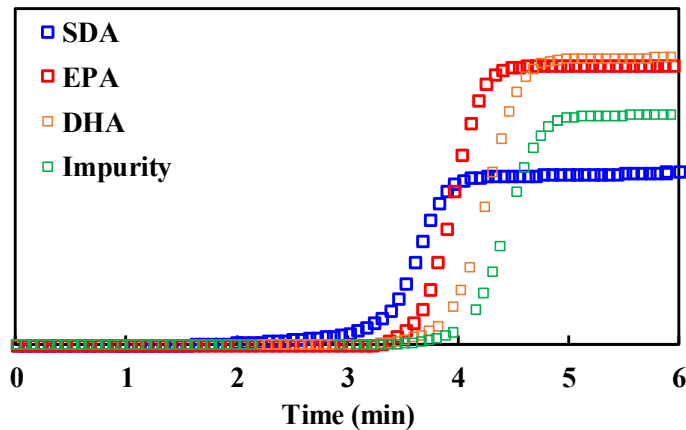
# Process Development: Single Column Chromatography

## STEP I: Single Column Chromatography

EPA is an intermediate retention component.  
Therefore, run the SMB twice.

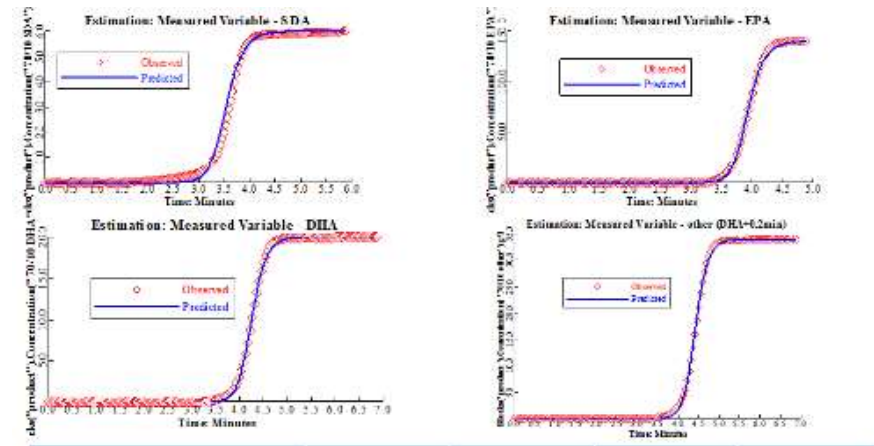
General rate model:

$$\frac{\partial c_{f,i}}{\partial t} + u \frac{\partial c_{f,i}}{\partial z} + \frac{(1-\epsilon_{total})}{\epsilon_{total}} \frac{\partial q_i}{\partial t} - D_{ax} \frac{\partial^2 c_{f,i}}{\partial z^2} + \frac{3k_i}{r_p} \cdot \frac{(1-\epsilon_0)}{\epsilon_0} \cdot (c_{f,i} - c_{p,i,r=r_p}) = 0$$



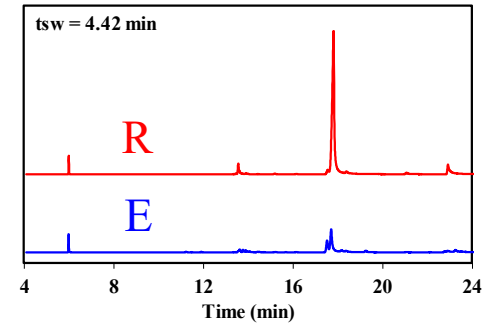
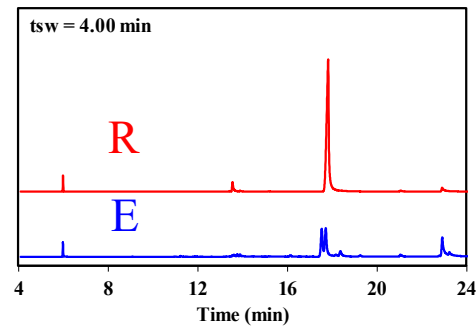
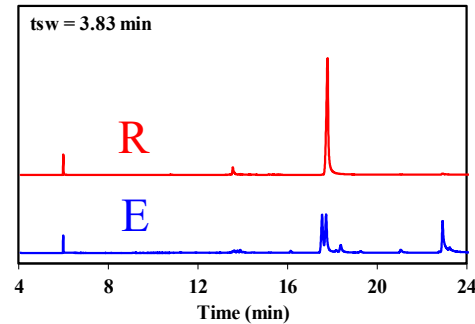
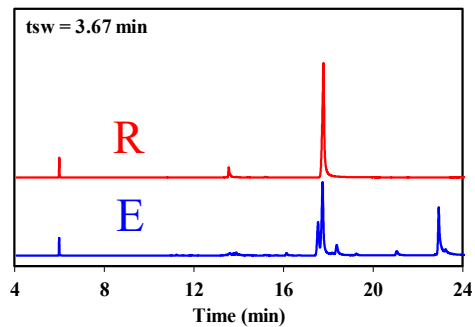
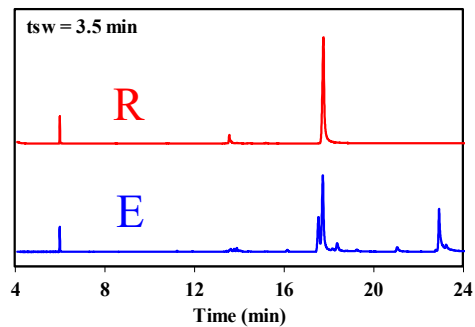
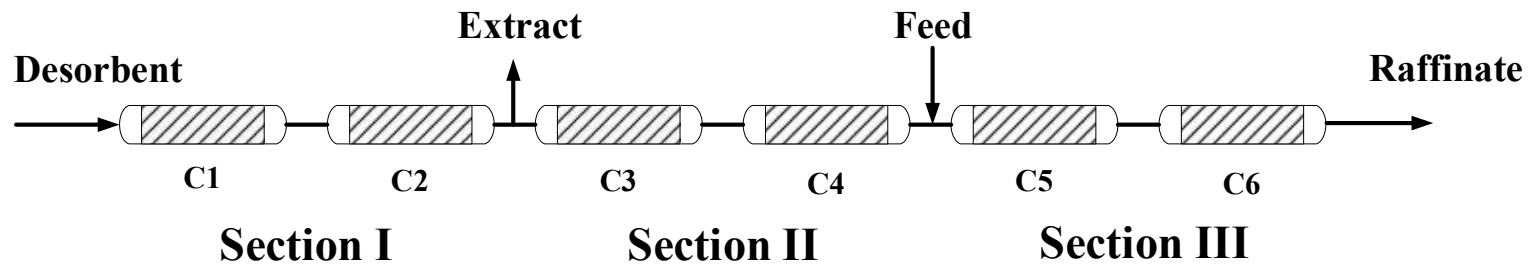
ASPEN Chromatography

- k = mass transfer coefficient
- d = dispersion coefficient
- IP1, IP2 = adsorption constants





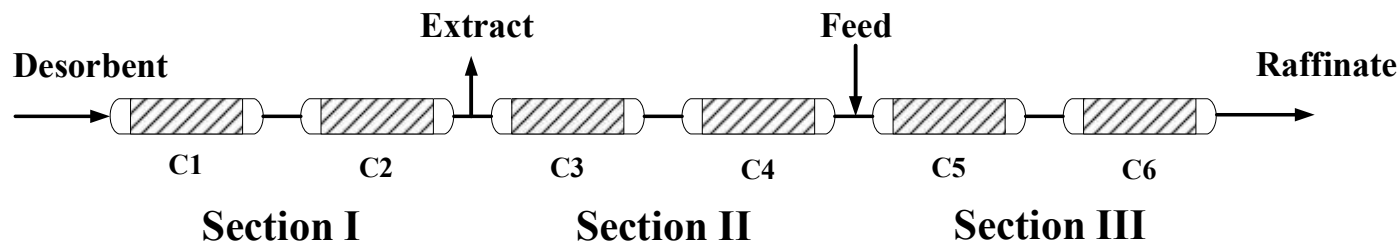
# Process Development: Results from Lab SMB



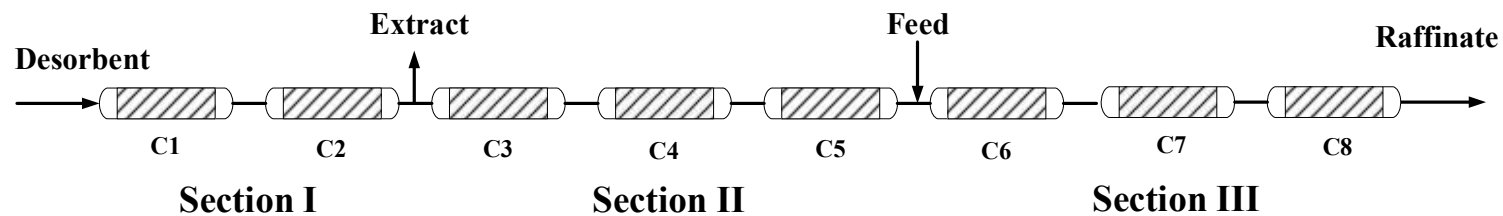


# Process Development: SMB Equipment

## Lab-scale SMB: 1 x 10 cm



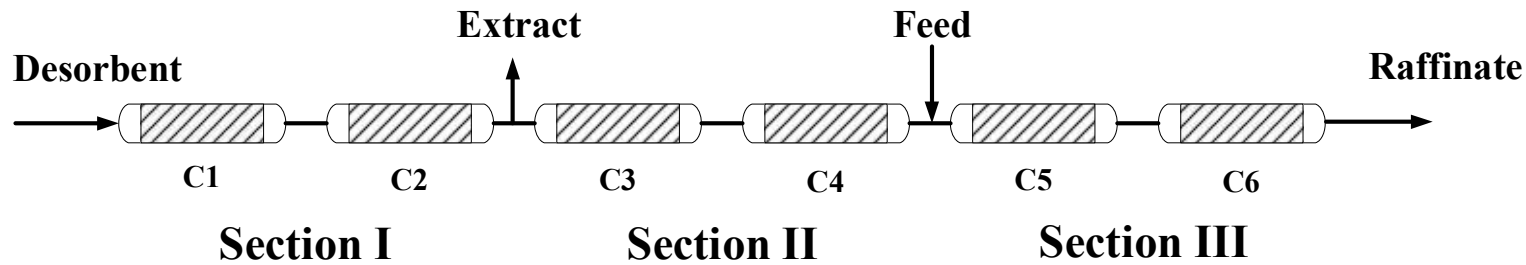
## Pilot-scale SMB: 3 x 25 cm



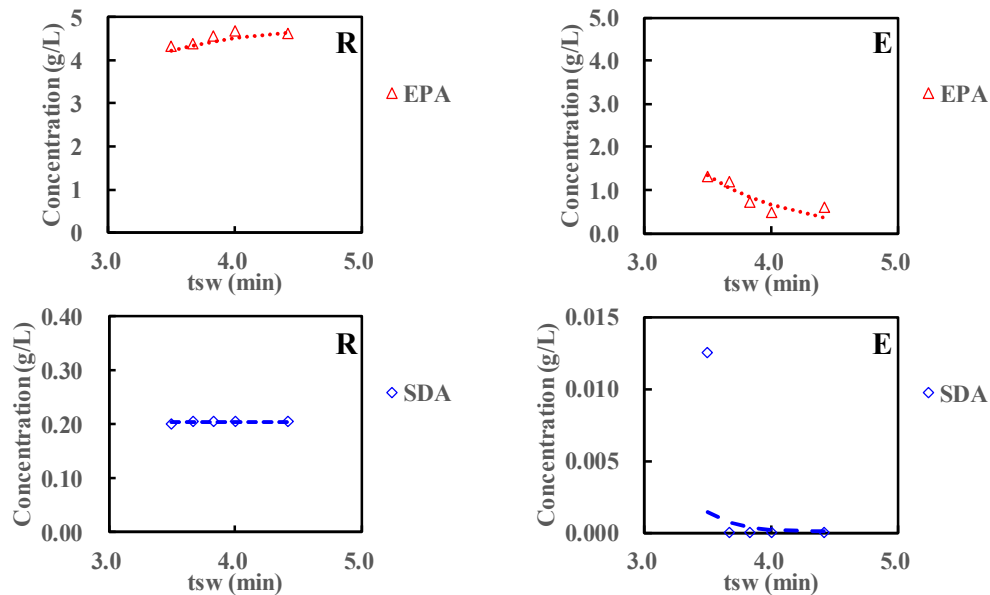


# Process Development: Results from Lab SMB

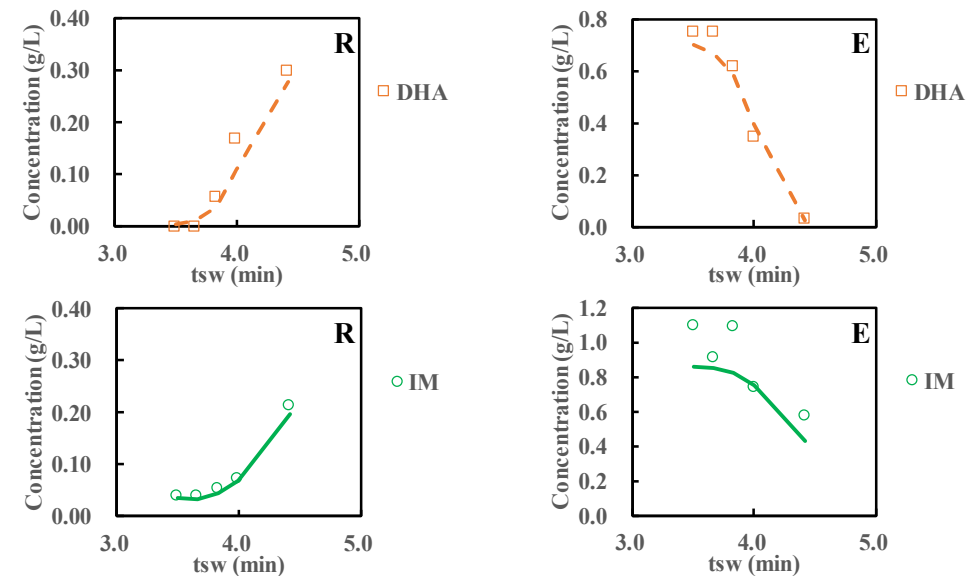
## Lab SMB: 1 x 10 cm



### 1st Run of SMB



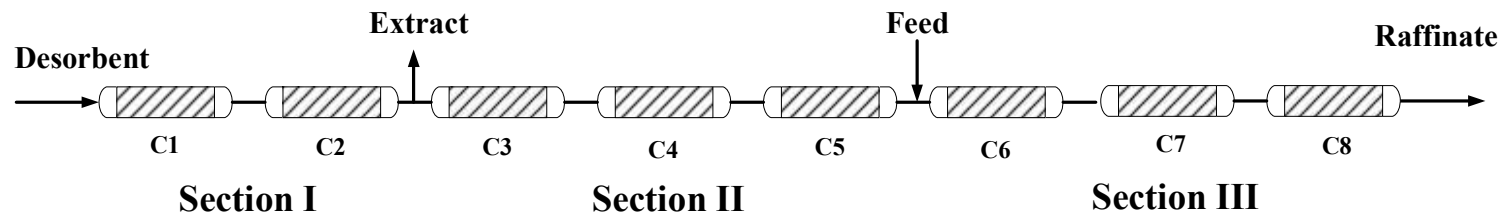
### 2nd Run of SMB



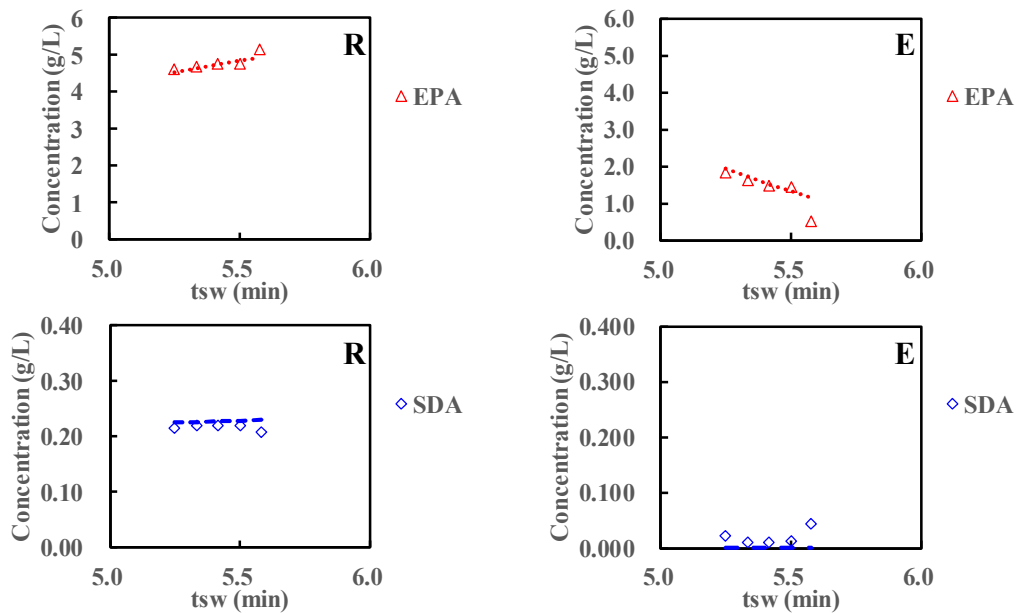


# Process Development: Results from Pilot SMB

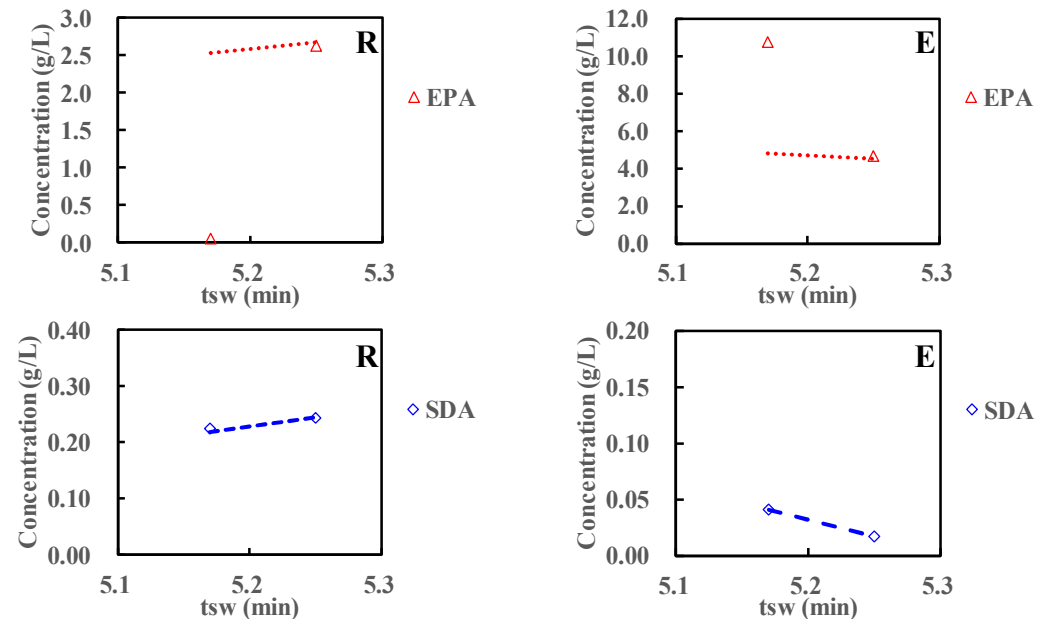
## Pilot SMB: 3 x 25 cm



### 1st Run of SMB



### 2nd Run of SMB





## Future Trends and Opportunities

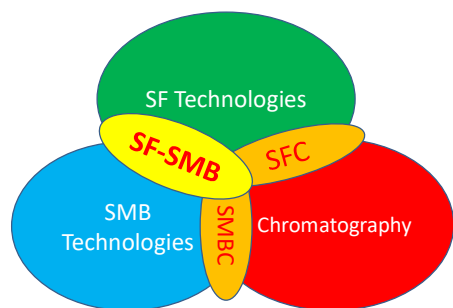
### Conclusions:

- The first of its kind of industrial application on SF-SMB has been realized in Taiwan for fish oil nutraceuticals.
- SF-SMB can be used to produce API(Active Pharmaceutical Ingredient) or ANI (Active Nutraceutical Ingredient).

### Challenges and Opportunities:

- Scale-up of the SF-SMB can further reduce the cost.
- SF-SMB needs sophisticated adsorbent for diversified application.
- Automation of SMB needs more studies and a new solid phase is always welcomed.
- **SF-SMB can also be applied in other products, such as chiral separation, natural product purification.**





# Thanks for Listening

